Amendments to the Claims:

The following listing of claims will replace all prior versions, and listings, of claims in the application:

- 1. (Currently Amended) Process for producing an integrally asymmetrical hydrophobic membrane having a sponge-like, open-pored, microporous support structure and a separation layer with a denser structure compared to the support structure, the process comprising at least the steps of:
- a) preparing a homogeneous solution from a system comprising 20-90% by weight of a polymer component eonsisting of comprising at least one polyolefin and 80-10% by weight of a solvent for the polymer component, wherein the system at elevated temperatures has a range in which it is present as a homogeneous solution—and on cooling has a critical demixing temperature, below the critical demixing temperature in the liquid state of aggregation has a miscibility gap, and has a solidification temperature,
- b) rendering the solution to form a shaped object, with first and second surfaces, in a die having at a die temperature above the critical demixing temperature,
- cooling the shaped object-using by contacting the shaped object with a liquid cooling medium that does not dissolve or react chemically with the polymer component at temperatures up to the die temperature, the liquid cooling medium being conditioned to a cooling temperature below the solidification temperature, at such a rate that a thermodynamic non-equilibrium liquid-liquid phase separation into a high-polymer-content phase and a low-polymer-content phase takes place and solidification of the high-polymer-content phase subsequently occurs when the temperature of the shaped object falls below the solidification temperature, and

d) possibly optionally removing the low-polymer-content phase from the shaped object, wherein

characterized in that a solvent for the polymer component is selected for which, on cooling at a rate of 1°C/min, the demixing temperature of a solution of 25% by weight of the polymer component in thethis solvent is 10 to 70°C above the solidification temperature. and that, for cooling, the shaped object is brought into contact with a liquid cooling medium that does not dissolve or react chemically with the polymer component at temperatures up to the die temperature.

- 2. (Currently Amended) Process <u>for producing a membrane</u> according to claim 1, <u>characterized in thatwherein</u> the solvent for the at least one polymer is one for which, for a solution of 25% by weight of the polymer component in <u>thethis</u> solvent and a cooling rate of 1°C/min, the <u>critical</u> demixing temperature is 20 to 50°C above the solidification temperature.
- 3. (Currently Amended) Process for producing a membrane according to claim 1 claim 2, wherein characterized in that the solvent for the at least one polymer is one for which, for a solution of 25% by weight of the polymer component in this solvent and a cooling rate of 1°C/min, the critical demixing temperature is 25 to 45°C above the solidification temperature.
- 4. (Currently Amended) Process for producing a membrane according to claim 1, wherein one or more of Claims 1 to 3, characterized in that the polymer component has a density of \leq 910 kg/m³.
- 5. (Currently Amended) Process for producing a membrane according to claim 1, whereinone or more of Claims 1 to 4, characterized in that the liquid cooling medium is a non-solvent for the polymer component that, on heating up to athe boiling point of the non-solvent, does not dissolve the polymer component to form a homogeneous solution.

- 6. (Currently Amended) Process for producing a membrane according to claim

 1, whereinone or more of Claims 1 to 5, characterized in that the liquid cooling medium is a liquid that is a strong non-solvent for the polymer component and is homogeneously miscible with the solvent at the cooling temperature.
- 7. (Currently Amended) Process for producing a membrane according to claim

 1, whereinone or more of Claims 1 to 6, characterized in that the liquid cooling medium has a temperature that is at least 100°C below the critical demixing temperature.
- 8. (Currently Amended) Process for producing a membrane according to claim

 1, wherein one or more of Claims 1 to 7, characterized in that 30-60% by weight of the polymer component is dissolved in 70-40% by weight of the solvent-system.
- 9. (Currently Amended) Process for producing a membrane according to claim

 1, wherein one or more of Claims 1 to 8, characterized in that the at least one polyolefin contained in the polymer component consists exclusively of carbon and hydrogen.
- 10. (Currently Amended) Process for producing a membrane according to claim 9, whereineharacterized in that the at least one polyolefin is a poly(4-methyl-1-pentene).
- 11. (Currently Amended) Process <u>for producing a membrane</u> according to claim 9, <u>whereineharacterized in that</u> the at least one polyolefin is a polypropylene.
- 12. (Currently Amended) Process for producing a membrane according to claim 9, wherein characterized in that the at least one polyolefin is a mixture of a poly(4-methyl-1-pentene) and a polypropylene.
- 13. (Currently Amended) Process for producing a membrane according to claim 10, wherein the solvent is characterized in that palm nut oil, dibutyl phthalate, dioctyl phthalate, dibenzyl ether, coconut oil, or a mixture thereof is used as the solvent.

- 14. (Currently Amended) Process for producing a membrane according to claim
 11, wherein the solvent is characterized in that N,N-bis(2-hydroxyethyl)tallow amine, dioctyl phthalate, or a mixture thereof is used as the solvent.
- 15. (Currently Amended) Process for producing a membrane according to claim

 1, wherein the membrane is one or more of Claims 1-to 14 for producing a hollow-fiber membrane.
- producible by a process according to <u>claim 1</u>, one or more of <u>Claims 1 to 15</u>, wherein the membrane consists <u>substantially essentially</u> of at least one polyolefin, has first and second surfaces and an intermediate support layer with a sponge-like, open-pored, microporous structure and adjacent to this support layer on at least one of <u>theits</u> surfaces a separation layer, where the separation layer is dense or has pores with an average diameter < 100 nm, the support layer is free of macrovoids, the pores in the support layer are on average substantially isotropic, and the membrane has a porosity in the range from greater than 30% to less than 75% by volume.
- 17. (Currently Amended) A gas separation process, comprising contacting a gas to be separated with the membrane made by the process of claim 1 Use of the membrane produced by a process according to one or more of Claims 1 to 15 for gas separation processes.
- 18. (Currently Amended) A gas transfer process, comprising contacting a gas with the membrane made by the process of claim 1 Use of the membrane produced by a process according to one or more of Claims 1 to 15 for gas transfer processes.

- 19. (Currently Amended) An oxygenation of blood process, comprising contacting blood with the membrane made by the process of claim 1 Use of the membrane produced by a process according to one or more of Claims 1 to 15 for oxygenation of blood.
- 20. (Currently Amended) An oxygenation of blood process, comprising contacting blood with the membrane of claim 16Use of the membrane according to claim 16 for oxygenation of blood.